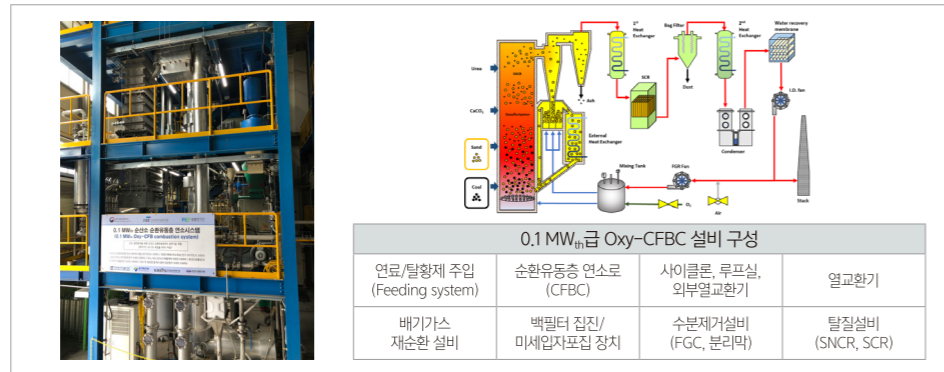


연료다변화 및 CO₂ 원천분리 가능 순환유동층 연소 기술

연소 중 CO₂ 원천분리가 가능한 연소 기술로써 연료 다변화가 가능하고 굴뚝으로 배출되는 배기가스량과 대기오염물질을 줄일 수 있는 기후변화 대응 친환경 순산소 순환유동층 연소* 시스템 기술.

*순산소 순환유동층 연소: Oxy-Circulating Fluidized Bed Combustion (Oxy-CFBC)

기술의 구성도/개념도



기술의 주요 내용 및 특징

- 연소 중 CO₂ 원천분리를 위한 power plant retrofit 기술(추가 공간 소요가 적음.)
- 순환유동층 연소로 내에서 탈황, 탈질 및 배기가스 재순환을 통한 후처리 비용 절감
- 연료 다변화/재료(층 물질, 부식 및 회분침적 방지)/탈황/탈질/집진/배기가스 내 물 회수 성능 시험평가 연소 설비로 활용 가능
- 순환유동층 연소 기술 활용 가능 분야
 - 화력발전 및 산업단지에서 배출되는 미연회분 재연소를 통한 시멘트 원료 생산
 - 국내 미이용 바이오매스 활용 에너지 생산(REC 확보)
 - 국외(베트남 등 동남아) 왕겨 활용 에너지 및 실리카 생산
 - 해양 폐플라스틱 처리 및 에너지 생산

기술의 적용처

응용분야	적용제품
발전소/산업단지/시멘트제조업/ 재료/폐기물처리 분야 등에 응용 가능	Oxy-CFBC / CO ₂ 원료 (CCU) / 전력, 스팀 / 시멘트 원료 / 왕겨 유래 실리카 / 폐플라스틱 처리 설비

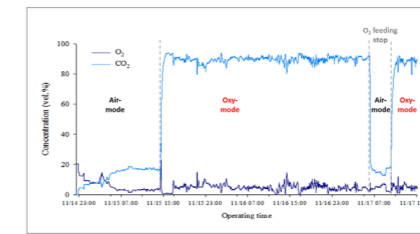
기술의 비교우위성/ 기존 기술 대비 차별성

실험 및 실증 데이터

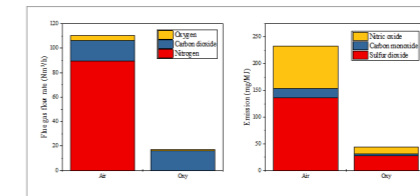
기술의 성숙도

지식재산권 현황

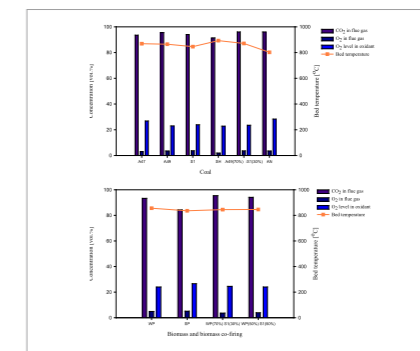
기존 기술	본 기술
<ul style="list-style-type: none"> 공기연소는 배기가스 내 N₂ 함량이 높아 CO₂ 분리/포집이 어려움. CO₂ 원천분리를 위한 순산소 연소 운전기법에 대한 기술 부족 	<ul style="list-style-type: none"> 국내 최초 배기가스 재순환 공정이 포함된 Oxy-CFBC test-rig 구축 및 운전기법 확보 배기가스 80% 감소(공기연소 대비) 연소효율 2% 향상(공기연소 대비) 90% 이상 CO₂ 원천분리 가능



공기 연소 ↔ 순산소 연소 전환 완료 시간: 40분 이내(배기가스 내 CO₂ 90 vol.% 이상 도달 기준)



배기가스 발생량: 공기 연소 대비 80% 감소
오염물질 배출량: 공기 연소 대비 SO₂ 80%, NO 85%, CO 76% 감소(정제설비 미가동)



연료다변화 테스트: 석탄(5종+혼탄1종) 및 바이오매스(2종+혼소2종) 순산소 연소 (무연탄, 갈탄, 아역청탄, 역청탄, wood pellet, straw pellet으로 대부분 5,000 kcal/kg 이하 연료 활용)



[TRL 4: 실험실 규모의 소재/부품/시스템 핵심성능 평가]

순산소 순환유동층 연소방식을 이용한 CO₂ 원천분리 및 대기오염 물질 감축 기술

· 0.1MW_{th}급 순환유동층 연소 공정 실험 [TRL 4 단계]

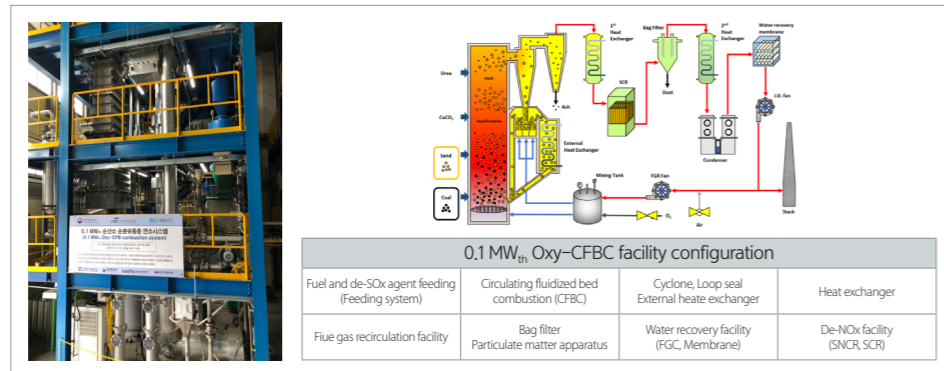
순번	발명의 명칭	출원번호	출원일자	등록번호	등록일자
1	순산소 순환유동층 연소장치의 연료다변화를 위한 저등급 연료 활용 시스템	10-2016-0071835	2016.06.09	10-1767188	2017.08.04
2	순산소 순환유동층 연소장치 및 이를 이용한 배기가스 재순환 방법	10-2017-0108075	2017.08.25	-	-
3	배기가스 재순환을 포함하는 안정적 물질 투입을 위한 순환유동층 반응기	10-2018-0052697	2018.05.08	-	-

Principal researcher
FEP Convergence
Research Center
Lee Jae-Goo

Oxyfuel circulating fluidized bed combustion (Oxy-CFBC) technology allowing for fuel diversification and CO₂ separation for carbon capture utilization and storage (CCUS)

Oxy-CFBC is the process of burning a fuel using pure oxygen with recirculated flue gas instead of air as a primary oxidant. It is also an eco-friendly combustion technology that allows the reduction of exhaust gas and air pollutants as well as the separation of CO₂ from the combustion without N₂ for CCUS.

Structural Diagram/Conceptual Diagram



Description and Characteristics of Technology

- Relatively easy retrofit from air to oxy mode system for CCUS and the requirement of small additional space
- Lower cost for air pollution control from in-situ desulfurization and denitrification inside CFBC via flue gas recirculation
- Utilization as a combustion facility for the performance tests such as fuel diversification, materials(Bed materials; prevention of corrosion and ash deposition), desulfurization, denitrification, dust collection, and water recovery from exhaust gas
- CFBC technology is applicable to the following areas:
 - Energy production by using unutilized domestic biomass
 - Production of energy and silica from rice husk from foreign countries (South East Asian countries including Vietnam)
 - Preparation of feedstock for cement production through reburning of unburned carbon(UBC) in ash from coal-fired power plant
 - Waste to energy plant(WtE)

Scope of Application

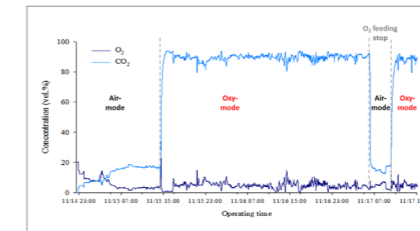
Application Fields	Products
Fuel diversified power plant (fossil fuel, biomass etc), CO ₂ capture in coal-fired power plant, WtE plant, Reburning process for UBC in fly ash	Power/CHP/CO ₂ for CCUS Waste plastic treatment facility/ Fly ash for cement feedstock/ Silica derived from rice husk



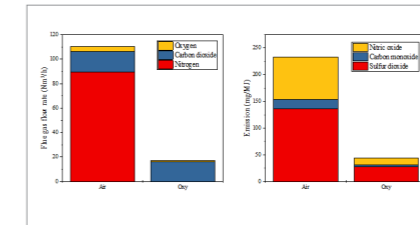
Comparative advantages of technology / Differentiation from existing technologies

Conventional Technology	Present Technology
<ul style="list-style-type: none"> • The high N₂ content in flue gas after air mode combustion makes CO₂ separation and capture difficult. • Larger amount of flue gas due to N₂ increases heat loss and the size of air pollution equipment 	<ul style="list-style-type: none"> • The Oxy-CFBC test-rig with flue gas recirculation has been established for the first time in Korea, and the operating technology · Exhaust gas decreased by 80% (compared to air-combustion) · Combustion efficiency increased by 2% (compared to air-combustion) · CO₂ separation more than 90%

Experimental and empirical data

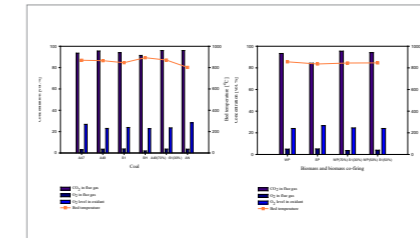


» The conversion between air-combustion and oxy-combustion requires less than 40 minutes (with reference to CO₂ over 90 vol.% in flue gas)



» The exhaust gas emission has been decreased by 80% compared to air-combustion.

» The pollutant emission has been decreased by 80% for SO₂, 85% for NO_x and 76% for CO compared to air-combustion (without operating the pollutant treatment facility).



» The fuel diversification has been tested through oxyfuel combustion of coal (five types + one mixed coal) and biomass (two types biomass + two types of mixed biomass with coal): Anthracite, Lignite, Sub-bituminous coal, Bituminous coal, Wood pellet, and Straw pellet; mostly below 5,000 kcal/kg).

Maturity level of technology



TRL 5: Preparation and performance evaluation with determined materials, parts, and system prototype

Technology for CO₂ separation and air pollutant emission reduction using oxyfuel fluidized bed combustion

• 0.1MW_{th} fluidized bed combustion process experiment [TRL 5]

No.	Title of Invention	Application Number	Application Date	Registration Number	Registration Date
1	System utilizing low rank fuel for diversification of fuel in Oxy-CFBC apparatus	10-2016-0071835	2016.06.09	10-1767188	2017.08.04
2	Circulating fluid bed combustion device and exhaust gas recirculation method using the same	10-2017-0108075	2017.08.25	10-1992296	2019.06.18
3	Circulating fluid bed reactor for stable material including flue gas recirculation	10-2018-0052697	2018.05.08	-	-
4	Dry exhaust gas recirculation type circulating fluidized bed combustion device and its operation method	10-2019-0059845	2019.05.22	-	-
5	Oxy circulating fluidized bed combustion apparatus for fly ash reburn and methods for operating	10-2019-0083537	2019.07.11	-	-

Current status of intellectual property rights

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